



RECOVERY OF SCANDIUM AND OTHER RARE EARTHS FROM GREEK BAUXITE RESIDUE

Dženita Avdibegović

KU Leuven, Belgium

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- 1 About the SIM² KU Leuven
- 2 Bauxite residue
- 3 Solvent extraction by ionic liquids (IL)
- 4 Sorption by supported ionic liquids (SILPs) and biopolymers

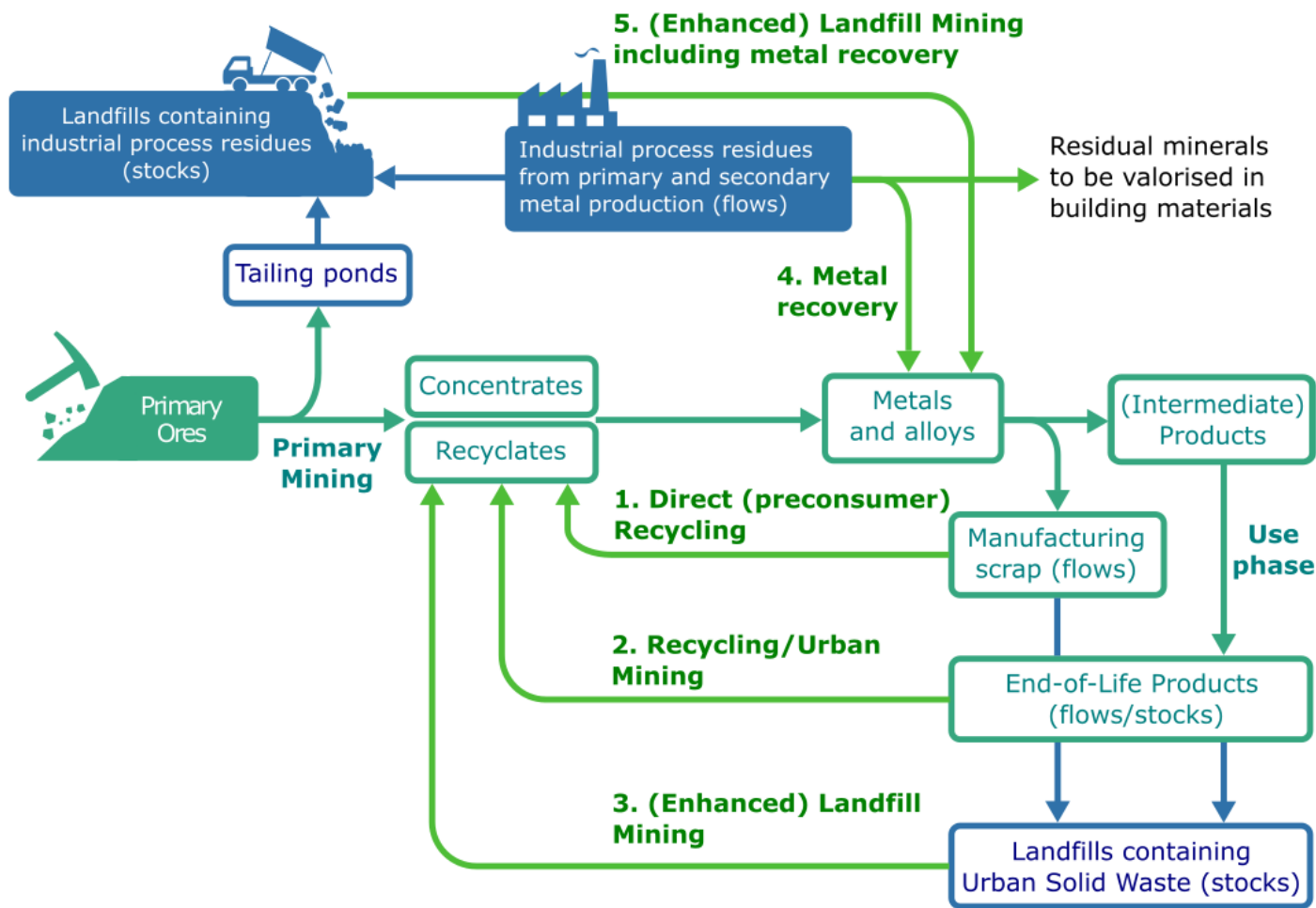


Who we are?

SIM² KU Leuven is a leading, interdisciplinary research cluster at KU Leuven uniting the research groups working on **Sustainable Inorganic Materials Management**.

<https://kuleuven.sim2.be>

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RESEARCH LINE 1

Geological exploration and advanced
resource characterisation

RESEARCH LINE 2

Pyro- and electrometallurgical
processes

RESEARCH LINE 3

Hydro- and solvometallurgical
processes

RESEARCH LINE 4

Upcycling processes for primary and
secondary resources

RESEARCH LINE 5

Sustainability Assessment and Policy
Research

RESEARCH LINE 6

Process intensification
and digitalisation

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SOLVOMET is KU Leuven's Centre set up to industrially valorise the expertise in solvometallurgy (incl. hydrometallurgy) that has been and is being developed in Prof. Koen Binnemans' research group (Department of Chemistry, KU Leuven, Belgium).



<https://solvomet.eu/>

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SYNTHESIS

Synthesis of new mining chemicals (extractants, diluents, adsorbents, collectors, flotation agents) for base and critical metal recovery and purification

CONCENTRATION & SEPARATION

- Solvometallurgical leaching
- Solvent extraction for separation and purification of base and critical metals
- Metal recovery from dilute aqueous waste streams by adsorption and ion flotation

SPECIATION

Development of more selective processes through a deeper understanding of the mechanism of solvent extraction processes

PROCESSES

Chemical engineering and mini-pilot-scale testing (upscaling) of developed processes and mining chemicals

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Bauxite residue = waste from the production of alumina by the Bayer process

- ✓ Estimated global production 150 millions of tonnes/year
- ✓ Bauxite residue is only rarely used in bulk quantities
- ✓ Presence of **Sc(III)** comprises more than 90% of its economic value of rare earth elements (REEs)



Greek bauxite residue
= 120 g/tonne of Sc

Compound	wt. %
Fe ₂ O ₃	44.6
Al ₂ O ₃	23.6
CaO	11.2
SiO ₂	10.2
TiO ₂	5.7
Na ₂ O	2.5

- ✓ The recovery of REEs with or without other metals from bauxite residue, and utilization of the left-over residue in other applications like building materials = contribution to a solution of the management problem of the bauxite residue.

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Compounds consisted exclusively of ions.

They can be organic or inorganic salts, with low melting temperature.

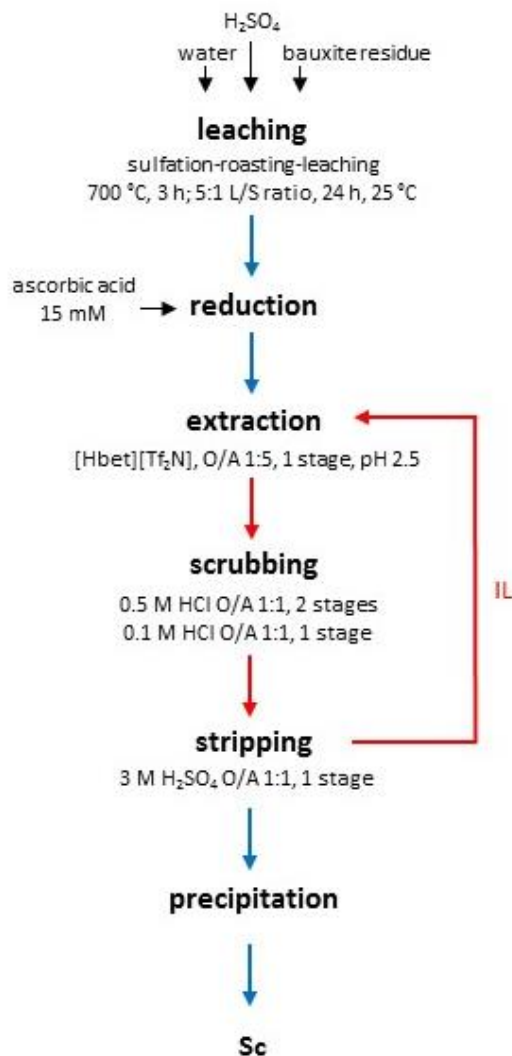
The most important properties:

- ✓ negligible vapor pressure,
 - ✓ broad electrochemical window,
 - ✓ low flammability,
 - ✓ broad liquidus range,
 - ✓ tunable structures (acidic groups for leaching)
-
- Designer solvents.



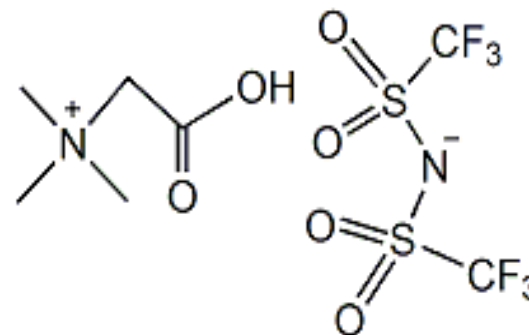
Ionic liquid process for Co/Ni separation (SOLVOMET)

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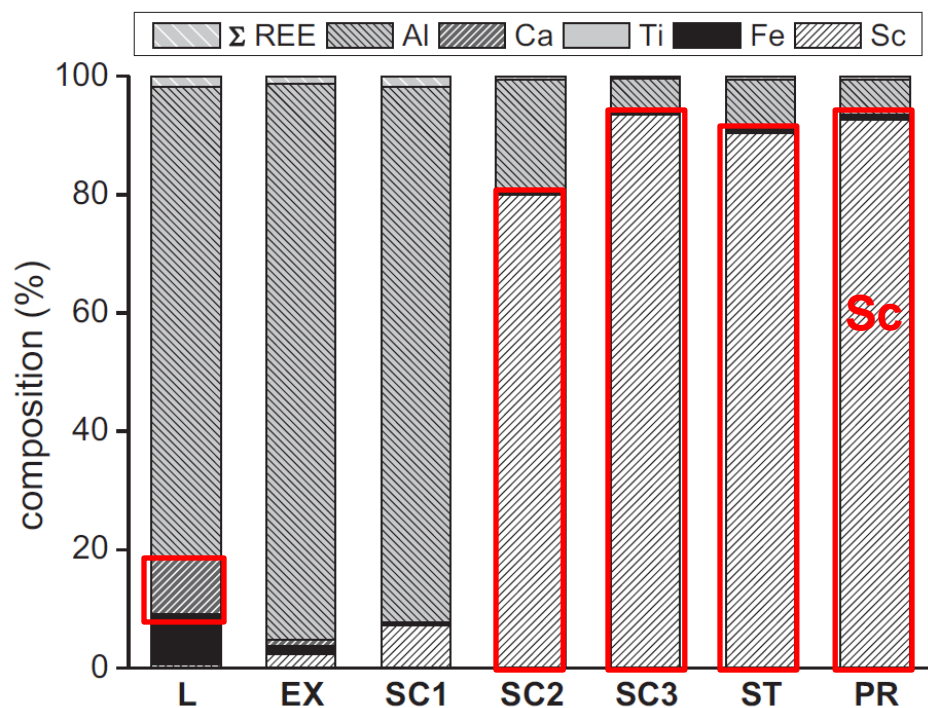


Betainium bis(trifluoromethylsulfonyl)imide [Hbet][Tf₂N]

Used for recovery of scandium from sulfation-roasted leachates of Greek bauxite residue by solvent extraction.



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L: sulfate leachate after 5-stage leaching,
 EX: ionic liquid phase after extraction
 SC1: IL phase after scrubbing step 1
 SC2: ionic liquid phase after scrubbing step 2
 SC3: ionic liquid phase after scrubbing step 3
 ST: aqueous phase after stripping
 PR: precipitate after precipitation with NaOH (pH 12.5).

Cycle	1	5
pH	3.12	3.08
Sc	14.6±0.2	47.7±0.1
Fe	59±1	271±1
Ti	<0.5	0.42±0.01
Ca	540±10	585±7
Na	3850±30	16100±6
Al	1078±1	4360±60
Y	12.7±0.2	25.1±0.1
La	16.0±0.2	25.1±0.1
Ce	44.4±0.8	53.8±0.3
Nd	11.0±0.1	11.5±0.1
Dy	2.09±0.01	2.65±0.01

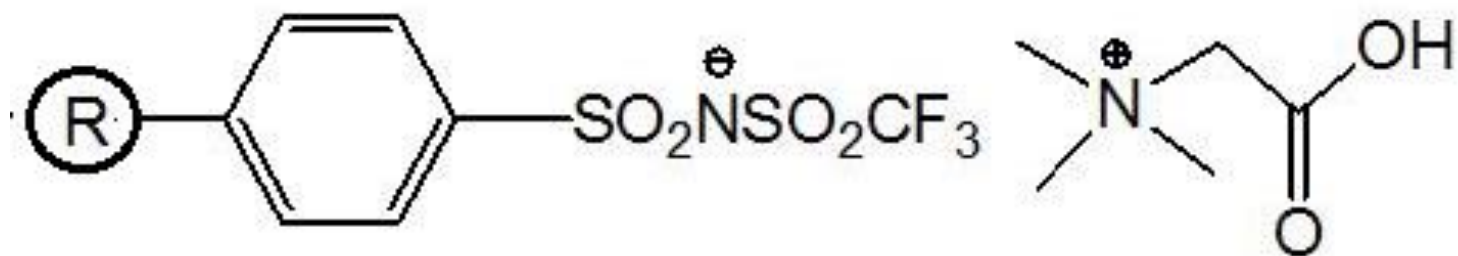
✓ Multi-stage leaching = increase the Sc concentration (mg L⁻¹) in the leachate.

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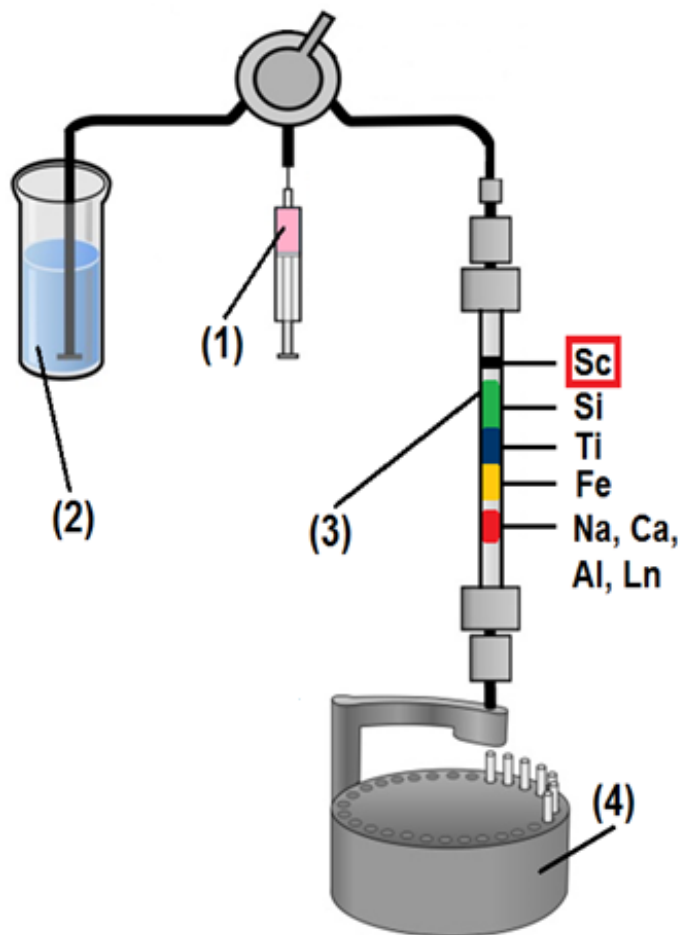
- The **viscosity** of ionic liquids is generally higher than that of common organic solvents.
- Supported ionic liquids (SILPs) were introduced to avoid the disadvantage of high viscosity of ionic liquids. SILPs include combination of ionic liquids and porous solid supports.

SILP betainium sulfonyl(trifluoromethanesulfonylimide) poly(styrene-co-divinylbenzene)

[Hbet-STFSI-PS-DVB]



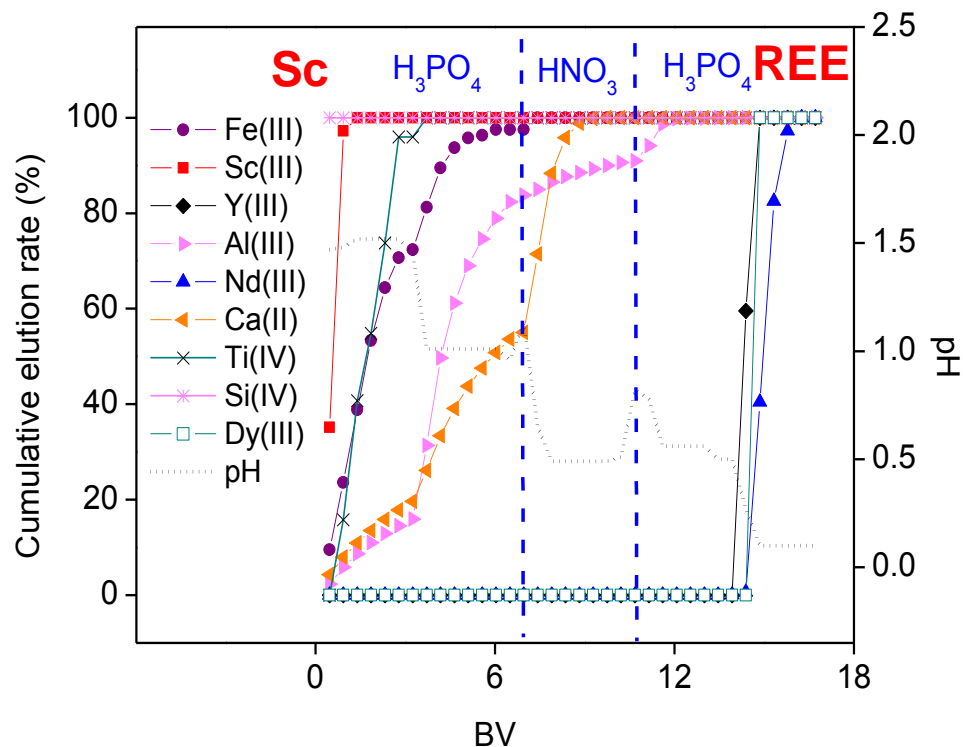
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- (1) = bauxite residue leachate
(2) = solution for removal of ions
(e.g. nitric acid)
(3) = column filled with sorbent
(e.g. SILP or biopolymers)
(4) = fraction collector

✓ High purification/preconcentration factors.

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SILP

Optimised pH gradient elution with H₃PO₄ and HNO₃ as a function of the bed volume (BV).

Feed 2 mL of BR leachate with HCl prepared from a BR slag performed after smelting reduction for Fe recovery.

pH_{ini}=1.5. Flow rate 0.5 mL min⁻¹.
Bed volume = 10.8 mL

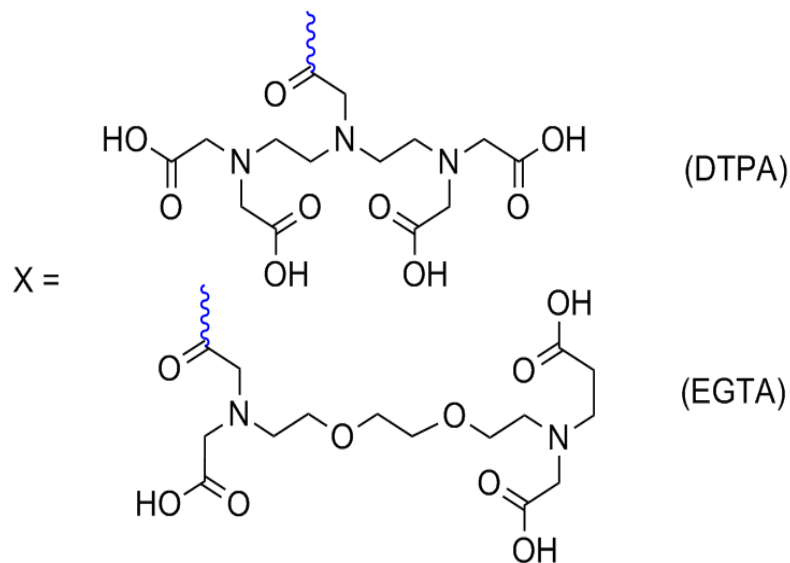
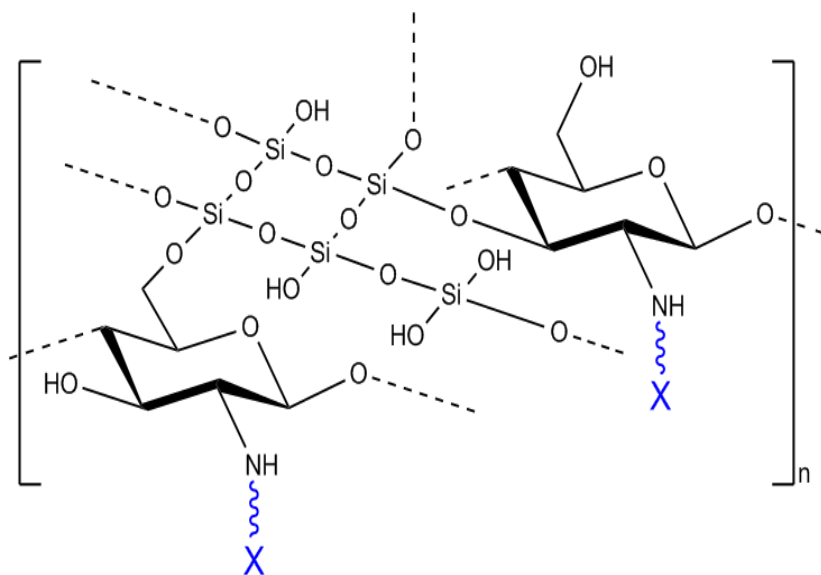
	Ca	Al	Fe	Si	Ti	Nd	Sc	Y	Dy
Concentration in the HCl feed (mg L ⁻¹)	4209	1972	518	49	3.3	7.7	1.0	7.5	0.9
Recovery by the SILP (%)	49.8	71.7	34.3	0.00	100	100	100	97.7	100

Elution sequence: Sc(III) > Fe(III) > Ca(II) > Al(III) ≈ Dy(III) ≈ Y(III) ≈ Nd(III).

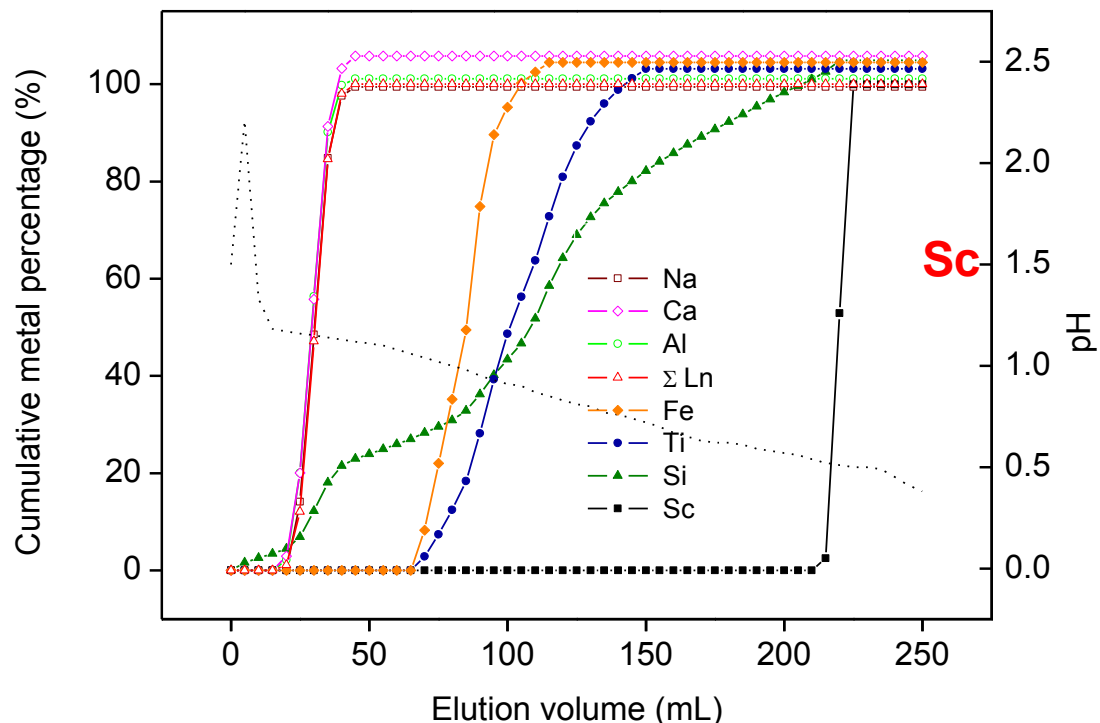
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Recovery of **Sc(III)** from leachate of Greek bauxite residue by functionalization of chitosan-silica with **EGTA**



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Biopolymers

Optimised pH gradient elution with HNO_3 as a function of the elution volume.

Feed 10 mL of BR leachate with HNO_3 .

$\text{pH}_{\text{ini}}=1.5$. Flow rate 40 mL h^{-1} .

Bed volume = 8.3 mL.

	Na	Ca	Al	Fe	Si	Ti	Sc	ΣLn
Concentration in the HNO_3 feed (mg L^{-1})	1104	939	670	106	558	106	2	6

Acknowledgement

Prof. Koen Binnemans (KU Leuven, Belgium)

Members of the ETN REDMUD Project

<http://redmud.org/>

<https://etn.redmud.org/>

Members of the SOLVOMET group

<https://solvomet.eu/>



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Thank you!

